

Super Boiler: Packed Media/ Transport Membrane (PM/TM) Boiler Development and Demonstration - (CPS #1458)

Goals: (1) Develop and demonstrate an advanced gas-fired package boiler with ultra-high efficiency, ultra-low emissions, and reduced footprint; (2) Formulate a long-range RD&D approach for advanced boiler technology.

Challenge: U.S. industry needs more efficient, cleaner, and more cost-effective steam generation technology.

Benefits: Reduced fuel use in gas-fired industrial package boilers; potential energy savings of 630 trillion Btu/year; NO_x reduction of 142,000 tons/year; space savings of 6 million sq ft.

FY05 Activities: Complete optimization of lab boiler and heat recovery system; design, build, install, and test a 10-MMBtu/h prototype; conduct field demonstration in southern California.



Participants: Gas Technology Institute, Cleaver-Brooks Div of Aqua-Chem, Pacific Northwest National Lab, Media and Process Technology.

Super Boiler: Packed Media/ Transport Membrane (PM/TM) Boiler Development and Demonstration - (CPS #1458)

Barrier-Pathway Approach

Barriers



- Inability to recover latent heat from boiler stack gases
- Inefficient NOx reduction methods for boilers
- Compact boiler design not compatible with NOx reduction *or* higher efficiency

Pathways



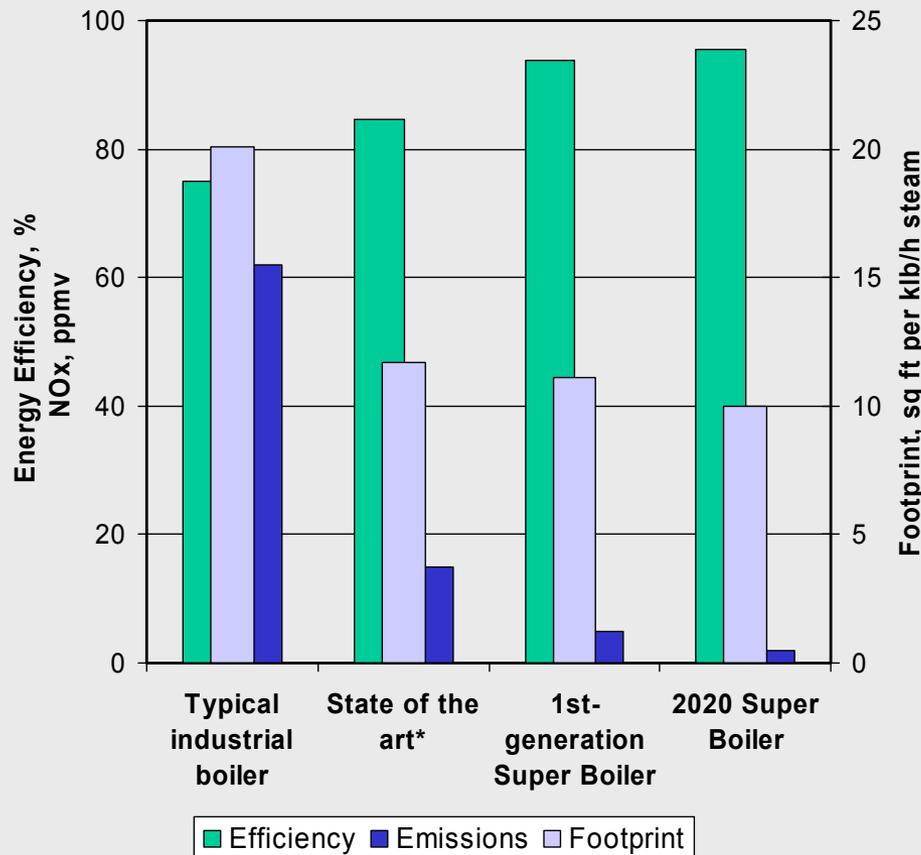
- Development of novel heat recovery system with transport membrane condenser
- Two-stage combustion system with interstage cooling and premixing
- Implementation of convective sections with extended surfaces

Critical Metrics

- Fuel-to-steam efficiency
- NOx, CO, VOC emissions
- Boiler footprint

Benefits (est)	2020
Energy saved	630 TBtu/y
NOx reduction	142,000 t/y
CO ₂ reduction	23 million t/y
Footprint reduction	6 million sq ft
Cost savings	\$4.0 billion/y

Boiler performance



- > Other key performance parameters
- Safety
 - Turndown
 - Responsiveness
 - Ease of operation
 - Time between outages
 - Availability
 - Capital cost
 - Maintenance cost
 - Life-cycle cost
 - Market acceptability

* Not all in the same boiler

Project team

- > Performing organizations
 - Gas Technology Institute
 - Cleaver-Brooks
- > Sponsors
 - U.S. Dept of Energy - Industrial Technologies Program
 - Southern California Gas Company
 - GTI Sustaining Membership Program
 - Gas Research Institute
 - Cleaver-Brooks
- > Other participants
 - Pacific Northwest National Lab
 - Media & Process Technologies
 - Dr. Jacob Korenberg

State of boiler R&D

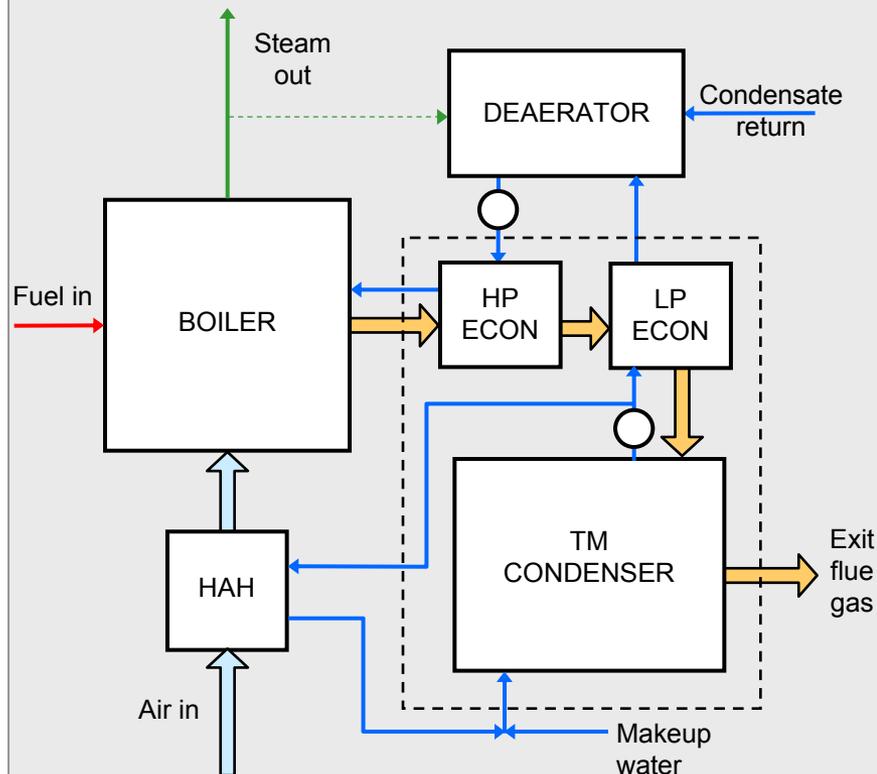
- > Identified 14 active R&D paths with potential application to steam generation
- > Formed Industrial Advisory Group
- > Drafted Super Boiler 2020 RD&D Plan

<i>Active R&D paths with Super Boiler potential</i>	
catalytic combustion	regenerative oxide-based combustion
direct steam generation	surface combustion
turbocharged boiler	improved boiler tube corrosion protection
water vapor pump	advanced heat exchangers
forced internal recirculation burner	ceramic burner components
high-swirl burners	electric field flame stabilization
oxygen enriched combustion	corrosion-resistant materials

1st Generation Super Boiler

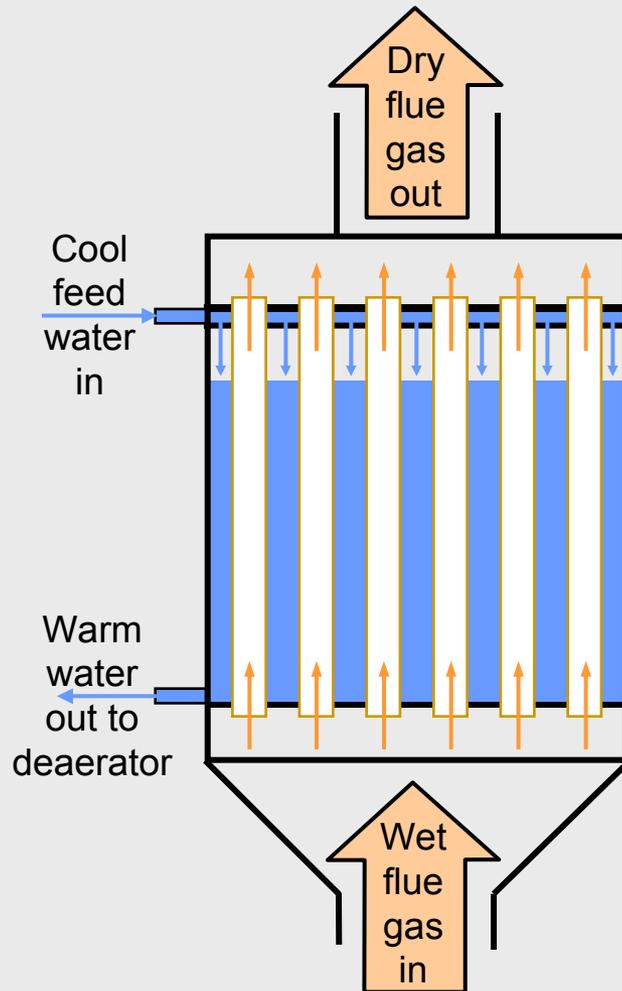
- > Design approach selected
 - Latent heat recovery from stack gases
 - Staged combustion with better temperature & combustion chemistry control in second stage
 - Advanced heat exchanger technology for compact design
 - Smart controls

Item 1: Heat Recovery



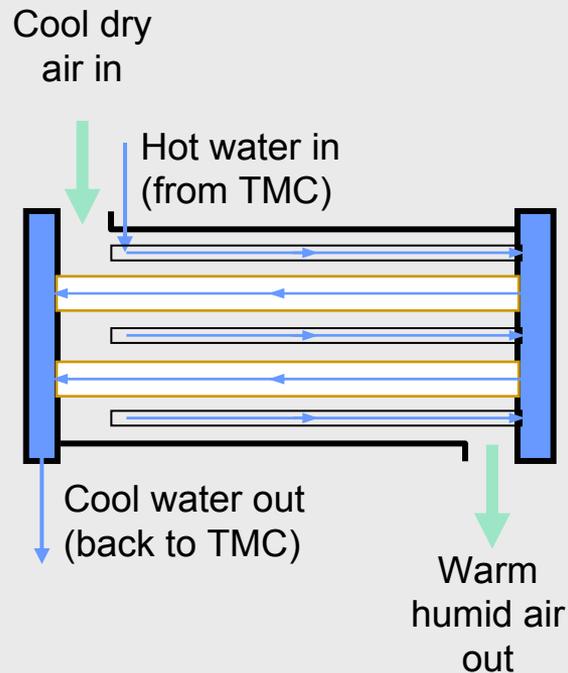
- > Compact staged economizers to remove sensible heat
- > TM condenser module using membrane technology to cool & dehumidify flue gas
- > Humidifying air heater (HAH) to cool and recycle TM condensate
- > Advanced controls to maintain optimal conditions

Heat Recovery: TM Condenser*



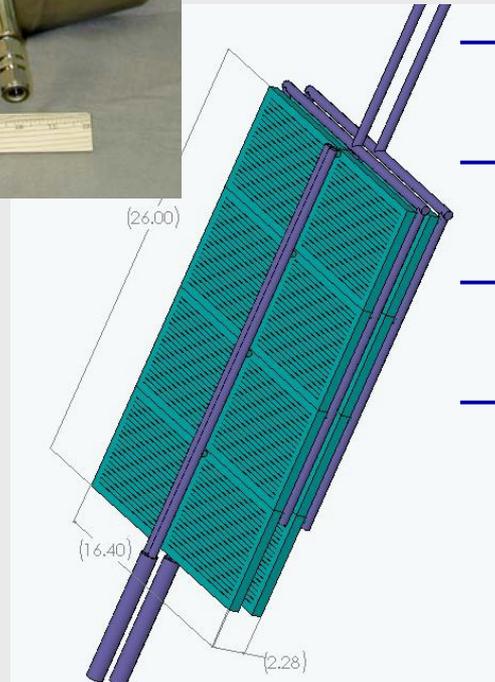
- > Selective transport of water vapor from flue gas to boiler feed water
- > Cools *and* dries flue gas
- > Transfers latent and sensible heat directly back to boiler energy loop
- > Flue gas exits below 130°F with no condensation
- > Feed water remains uncontaminated

Heat Recovery : Humidifying Air Heater



- > Microporous ceramic membrane tubes
- > Hot water first transfers heat to combustion air
- > Partly cooled water passes through membrane to humidify combustion air
- > HAH cools water for TM condenser and improves performance

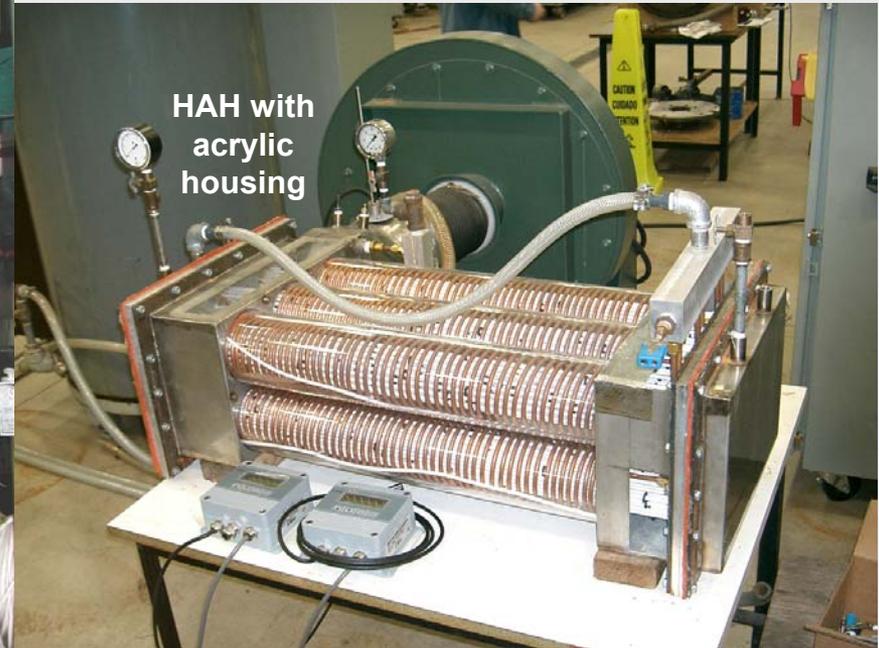
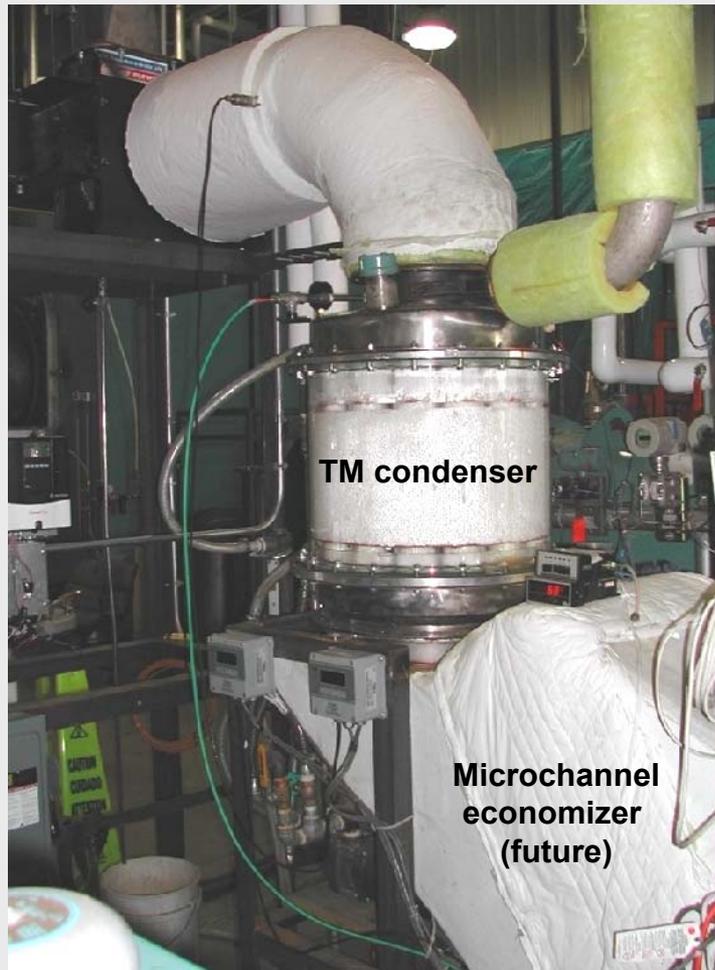
Heat Recovery: Microchannel Economizer



- > PNNL microchannel heat exchanger
 - Tested on 60,000 Btu/h combustor
 - Tested as steam generator or economizer
 - Can be made from variety of materials
 - Volumetric heat transfer increased up to 65-fold*
 - Full-scale (3-MMBtu/h) prototype under construction

* 912,000 Btu/h/ft³ versus 14,000 Btu/h/ft³ for conventional economizer

Heat Recovery: TM condenser & HAH

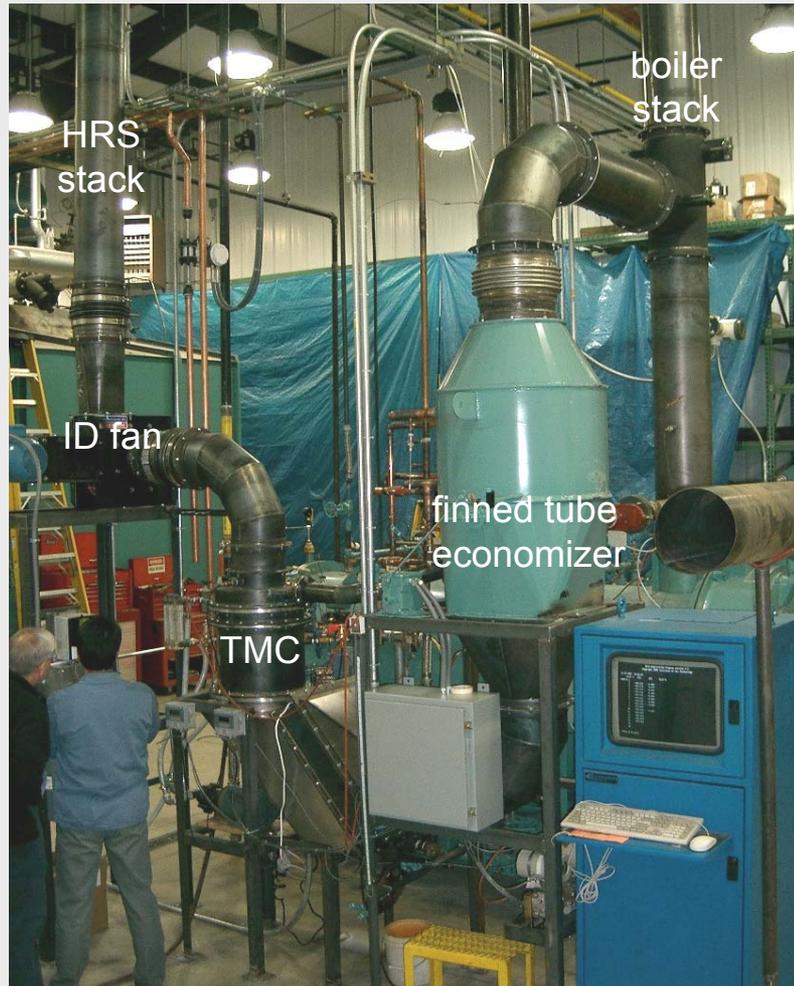


Heat Recovery: Predicted Energy Efficiency

Case	Cond return (%)	Comb air temp (°F)	Stack temp (°F)	Stack dew pt (°F)	Efficiency (%)
1	None	134	120	102	95.2
2	25	132	132	114	93.5
3	50	120	141	123	91.8
4	75	95	149	131	90.0

- Natural gas: 93.7%CH₄, 2.8%C₂H₆, 0.6%C₃H₈, 2%N₂, 0.9%CO₂
- ISO combustion air (60%RH at 59°F)
- 10% excess air combustion
- 60°F makeup water
- 180°F condensate return

Heat Recovery: Lab testing system



Heat Recovery Data:

Single economizer + TM condenser

Firing rate	1.75 MMBtu/h	3.00 MMBtu/h
Stack O ₂ , vol%	4.6%	2.8%
Gas temp, economizer inlet	325°F	317°F
" " economizer outlet	178°F	169°F
" " TM condenser outlet	122°F	125°F
Gas dew point, TM condenser inlet	131°F	131°F
" " " TM condenser outlet	117°F	119°F
Water temp, TM condenser inlet	57°F	72°F
" " TM condenser outlet	125°F	115°F
Water removed from flue gas	39.1% of total	36.3% of total
Calculated boiler efficiency	92.1%	92.3%

Item 2: Heat Transfer

- > Shorten convective passes
 - Firetubes with internal extended surfaces
 - Heat transfer up to 18 times more intensive than rifled tubes
 - 2-pass boiler can deliver efficiency of 4-pass design with smaller size and lower cost

Heat Transfer: Estimated Size Reductions

	Design case		
% relative to base case	#1	#2	#3
Footprint	61	75	70
Cross-section	71	56	50
Volume	51	56	49
Weight	51	59	51

- > Conventional boiler base case:
 - 10-MMBtu/h (250 hp)
3-pass firetube boiler
w/450°F flue gas
 - 88" shell ID, 127-ft²
footprint, 728-ft³ volume,
11.2-ton dry weight
- > Equivalent capacity and heat removal
- > Compliant with NO_x emissions target

Laboratory Boiler: Single-stage boiler

- > Extended-surface firetube heat transfer testing
- > Pressure vessel design evaluation
- > Flue gas for heat recovery testing
- > Installation/shakedown completed Dec 2003
- > Testing
 - ✓ Heat transfer & pressure drops
 - ✓ General mechanical performance
 - ✓ Heat recovery system



Heat Transfer Data: 1-stage 2-pass lab boiler

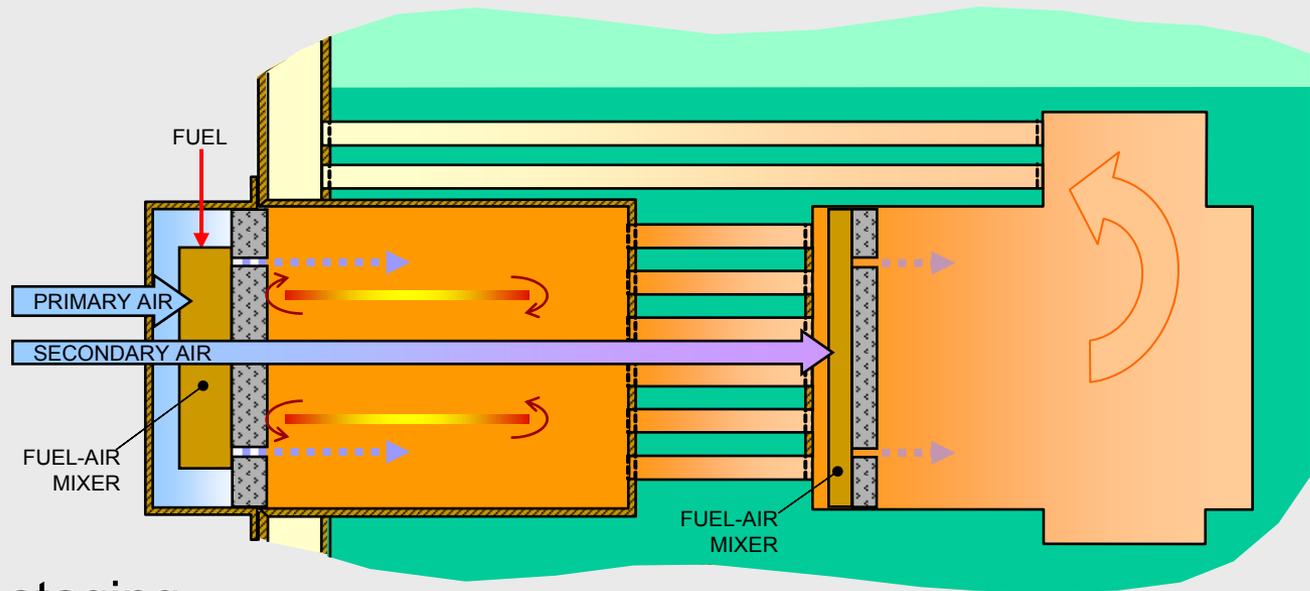
Firing rate, MMBtu/h	Firetube version	Conv pass ΔP , inwc	Sat steam temp, °F	Stack temp, °F	DT, °F
2.1	A	1.6	342	431	89
3.0	A	3.5	343	489	146
2.1	B	3.3	343	357	14
3.0	B	5.4	342	377	35

Laboratory Boiler: Two-stage boiler

- > Combustion & integrated system testing
- > Heat transfer optimization
- > Installation/shakedown completed Feb 2004
- > Started testing March 2004
 - ✓ Combustion performance
 - ✓ Heat transfer & pressure drops
 - ✓ Controls



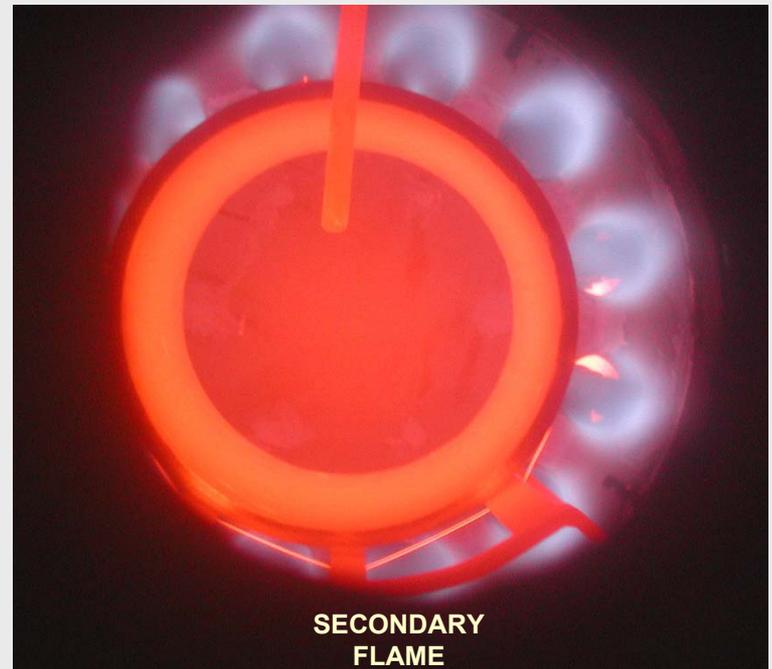
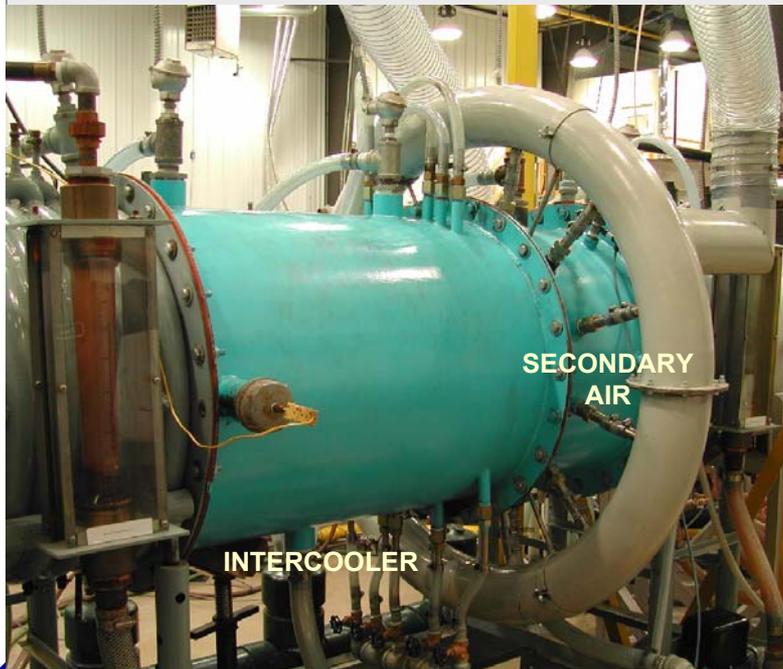
Item 3: Combustion



- > Air staging
- > Forced internal recirculation insert
 - Increases heat flux to water walls
 - Anchors and stabilizes flame
- > Premixed fuel/air in both stages
- > Interstage heat removal
 - Reduces 2nd-stage flame temperature

Combustion: 2-Stage design development

- > Boiler simulator tests
 - Fired at 2 to 10 MMBtu/h (5:1 turndown)
 - NO_x below 5 vppm with good burnout at low excess air
 - High combustion intensity w/short secondary flame



Combustion Data:

2-stage lab boiler emissions

Firing rate, MMBtu/h	O ₂ , vol%	NO _x , vppm*	CO, vppm*	HC, vppm*
0.85**	7.2**	8.2**	14**	2**
1.70	2.0	2.2	6	0
2.52	3.4	3.3	5	7
3.00	3.0	2.6	7	0
3.65	2.1	3.0	7	0

3.0-MMBtu/h
secondary flame



Heat Transfer Data: 2-stage 2-pass lab boiler

Firing rate, MMBtu/h	Furnace 1 temp, °F	Furnace 2 temp, °F	Conv pass ΔP , inwc	Steam temp, °F	Stack temp,* °F
0.85*	1385	702	0.5	220	200
1.70	1222	1912	1.0	339	314
2.52	N/A	N/A	2.5	348	346
3.00	1853	2049	2.7	349	354
3.65	1941	2146	3.3	349	367

* Light-off - single-stage (fuel-lean) firing

** Does not account for heat loss from uninsulated stack nozzle

Design issues: Combustion

- > Fan requirement
- > Safety
 - Flame sensing
 - Air-fuel ratio control
- > Turndown
 - 4:1 minimum, 6:1 desirable
- > Responsiveness
 - Ramp rate & hysteresis
 - Maintain compliance during transitions
- > Operability
 - Fully automatic unattended operation
- > Backup fuel
 - No. 2 oil

Design issues:

Heat transfer

- > Code compliance
- > Pressure drop
- > Long-term durability
 - Corrosion
- > Maintenance & cleaning
- > Backup fuel
 - Compatibility
 - Cleanability

Design issues:

Heat recovery

- > Code compliance
- > Control strategy
 - Simplicity
 - Load-following capability
- > Long-term durability
 - Membranes
 - Corrosion avoidance
 - Pumps, valves, and sensors
- > Maintenance
 - Cleanability
 - Backup fuel

Progress and outlook

- > Complete lab testing
 - Optimize combustion performance
 - Validate computer models for scale-up
 - Optimize heat recovery system performance
 - Optimize control strategy
- > Field demonstration
 - Select best design features from lab testing
 - Select a Southern California host site
 - Design and build commercial prototype boiler
 - Conduct field demonstration
- > Commercialization
 - Additional field demonstrations
 - Introduce into commercial and light industrial market